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Hot-wire anemometry for superfluid turbulent coflows

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We report the first evidence of an enhancement of the heat transfer from a heated wire to an external turbulent coflow of superfluid helium. We used a standard Pt-Rh hot-wire anemometer and overheat it up to 21 K in a pressurized liquid helium turbulent round jet at temperatures between 1.9 K and 2.12 K. The null-velocity response of the sensor can be satisfactorily modeled by the counterflow mechanism, while the extra cooling produced by the forced convection is found to scale similarly as the corresponding extra cooling in classical fluids. We propose a preliminary analysis of the response of the sensor and show that—contrary to a common assumption—such sensor can be used to probe local velocity in turbulent superfluid helium. © 2015 AIP Publishing LLC. [<http://dx.doi.org/10.1063/1.4913530>]

I. INTRODUCTION

At temperatures below $T_\lambda \approx 2.18$ K, liquid helium undergoes a phase transition, from a classical fluid (He I) to quantum one (He II). The latter phase exhibits many peculiar properties among which the ability to flow without apparent dissipation through thin capillaries, the quantization of the vorticity in atomic-diameter vortex filaments, and a very efficient heat transport associated with the existence of temperature waves (“second sound”).¹ Those properties are well understood in the framework of the two-fluid model: He II is described as a mixture of a “normal” and a “superfluid” components. The first one is viscous and carries all the entropy of the fluid, while the second is inviscid and irrotational except on the quantized line vortices.

The present work was motivated by the experimental study of turbulence^{2,3} in He II, and associated velocity sensors. In particular, the study is focused on mechanically driven and pressure driven flows, also called coflows (as opposed to thermally driven He II called counterflows that have no equivalent in classical fluids). A common picture of classical turbulent motion is the Richardson cascade: the largest eddies of the flow are continuously stretched producing smaller and smaller eddies with no significant energy loss in the “cascade” process. This process holds until eddies are small enough for the viscous dissipation to become significant. A good illustration of this process is given by the distribution of the kinetic energy as a function of the flow scale. In He II, at large scale, experimental, theoretical, and numerical works (see, e.g., Ref. 4 for a review) indicates that the two components of He II are locked (through the so-called “mutual friction term”) and exhibit Kolmogorov-like power spectra. Unfortunately,

the smallest scales of turbulent coflows are far from being resolved by the existing velocity sensors.

To the best of our knowledge, only two major velocity measurement principles were applied to He II: (i) stagnation pressure measurements, such as total head pressure tubes,^{5,6} Pitot tubes,^{6,7} or cantilevers⁸; (ii) particle visualization methods among which Laser Doppler Velocimetry,⁹ Particle Image Velocimetry,¹⁰ and Particle Tracking Velocimetry^{11,12} down to scales even smaller than the inter-vortex spacing.

One of the most commonly used velocity sensors in classical turbulence is absent from the above list: the hot-wire. The popularity of hot-wires in the field of hydrodynamics is due to their very high spatial and temporal resolution (see, e.g., Refs. 13 and 14 for extreme miniaturization). Such sensors have already proven to be very useful at cryogenic temperatures (e.g., Refs. 13, 15–17), in particular for the study of very high Reynolds number turbulence in gaseous helium. However, it is often assumed that hot-wires cannot work in He II.¹⁸ Their measurement principle is based on the heat transfer enhancement when a heated wire is submitted to forced convection. In classical fluids, at length scales typical of hydrodynamic experiments, the forced convection is much more efficient than natural convection and molecular diffusion. However, in superfluid helium, another very efficient thermal transfer mechanism comes to be even more efficient than forced convection. Physically, this mechanism is associated with the generation of a counterflow between the normal and superfluid components of He II (respectively, subscripted n and s hereafter). The normal component flows outward, carrying its entropy away from the heat source, while the entropy-less superfluid component flows inward and ensures net mass conservation. The efficiency of this heat transfer mechanism is limited by the generation of a superfluid vortex tangle self-sustained by the counterflow itself. Nevertheless,

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even for large heat fluxes, that produce large vortex line densities, the counterflow mechanism stands very efficient, and forced convection does not improve significantly the heat transfer.¹⁹ For instance, hybrid magnets can be cooled by static He II²⁰ (p. 54), even with long distances between the thermal source and sink.

The need for time and space resolved velocity measurements has led us to analyze to which extent the heat transfer improvement due to forced convection in He II can be resolved. A standard Ag coated Pt–Rh Wollaston wire driven by a commercial constant temperature anemometer was used to investigate the effect of forced convection on heat transfer in He II. In this article, we show that the response of the sensor can be successfully used as a local velocity measurement. After a brief description of the experimental apparatus, we first analyze the static response of the sensor, i.e., without external flow. The standard approach for describing heat transfers in He II, is found to satisfactorily predict the response of the sensor. In the presence of an external flow, we observe an enhancement of the heat transfer. We present 3 experimental evidences that the local velocity of the external flow is responsible for the enhancement.

II. MEASUREMENT SETUP

A. Wind tunnel

The experiment is performed in a pressurized cylindrical vessel ($\varnothing 200 \text{ mm} \times 500 \text{ mm}$), where a liquid helium round jet develops from a nozzle with inside diameter $D_n = 5 \text{ mm}$ (see Ref. 21 for details). The temperature can be continuously varied from 4.2 K to 1.7 K, so that classical (He I) and superfluid (He II) flows can be achieved in the same apparatus, respectively, above and below the superfluid transition temperature $T_\lambda \approx 2.17 \text{ K}$. The pressure is kept greater than the helium critical pressure ($P_C \approx 2.2 \text{ bars}$) in order to avoid the onset of boiling at the surface of the hot-wire.

The hot wire is located on the axis of the jet, at $45 \times D_n$ or $60 \times D_n$ downstream from the nozzle. In this region, classical turbulence literature (see, e.g., Ref. 22) show that most of the quantities of interest such as the velocity and its first moments, the integral length scale and the Taylor's length scale, are self-similar. As we could not map the velocity field of the jet, we assumed classical behavior so that the velocity at a particular distance from the nozzle is assumed to follow the same scaling as in Wignanski and Fiedler.²² This assumption is supported by the fact that we found a quantitative agreement between the expected integral time and the auto-correlation time of the signal at various Reynolds numbers both in He I and He II.

The mean velocity U_{45D} or U_{60D} seen by the wire is varied typically from 0.1 up to 1.5 m/s, corresponding in He I, to Reynolds number up to $Re = U_{0D}D_n/\nu \approx 1 \times 10^6$ where ν is kinematic viscosity of He I.

B. Hot-wire

The probes are manufactured using standard Platinum–Rhodium (90% Pt–10% Rh) Wollaston wires of diameter $1.3 \mu\text{m}$. The length of the sensitive etched part of the wires is

$l_w \approx 400 \mu\text{m}$. The wire is welded on the stainless steel prongs of a home made ceramic mounting.

From room temperature down to few tens of Kelvins, the resistivity $\rho(T)$ of Pt–Rh alloy decreases linearly with temperature. Below 30 K, the temperature dependence roughly vanishes as $\rho(T) \approx \rho_0(1 + 2 \cdot 10^{-8} T^4)$, where the residual resistivity ρ_0 is interpreted as being due to the presence of defects and impurities in the material (here ρ_0 corresponds to $R_{\text{wire}} \approx 50 \Omega$). The hot wire was overheated at a temperature set within $T_w = 20\text{--}25 \text{ K}$. In those conditions, the fluid that surrounds the wire undergoes a steep but continuous density and temperature variation. We have checked, in He I, that electrical response of the hot-wire did not show peculiar characteristics due to this very high temperature difference with regards to the surrounding fluid temperature: the usual Kings calibration law holds down to the lowest velocities explored with He I.

The wire is driven at constant resistance (“Constant Temperature Anemometry” or CTA mode) using a commercial DISA-55-M10 CTA anemometer bridge. The output voltage signal of the anemometer is proportional to current required to overheat the hot-wire up to the setup resistance (i.e., temperature). The resistance control system was checked to be reliable up to frequencies of order 10 kHz so that the results presented hereafter are low-pass-filtered at 5 kHz.

The signals were acquired either on a NI-PXI4462 or a HP-E1430 acquisition boards, at sampling frequencies up to 100 kHz. For one velocity measurement, typical data set was 30 files with 2^{22} points. This corresponds to 4000 integral times at the highest velocities.

III. RESULTS

A. DC response of the hot-wire

The continuous line of Figure 1(a) presents the mean heat flux φ_0 at the surface of the hot-wire as a function of bath temperature when the jet is turned off and the wire regulated at $T_w \approx 21 \text{ K}$. Right below the superfluid transition ($T_\lambda \approx 2.15 \text{ K}$ at 2.6 bars), the heat flux rises sharply, with a 5 fold increase between T_λ and 1.9 K. To discard possible artifact of the regulation electronics, this measurement has been reproduced independently in open-loop mode, by manual adjustment of an independent voltage source driving the hot-wire (filled circles). For later discussion, it is convenient to introduce here the bath-temperature sensitivity γ of the hot-wire heat flux φ_0 :

$$\gamma = \frac{1}{\varphi_0} \frac{d\varphi_0}{dT_{\text{bath}}} . \quad (1)$$

Over the explored temperature range, typically $\gamma \approx -2 \text{ K}^{-1}$.

The observed velocity dependence of the heat flux φ (averaged over the whole wire surface) can be written in the same form as in classical fluids:

$$\varphi = \varphi_0 + Bv^\alpha , \quad (2)$$

with $\alpha \approx 0.5$ in the general case due to the $v^{-0.5}$ scaling of the thermal boundary layer thickness. While in He I data (not

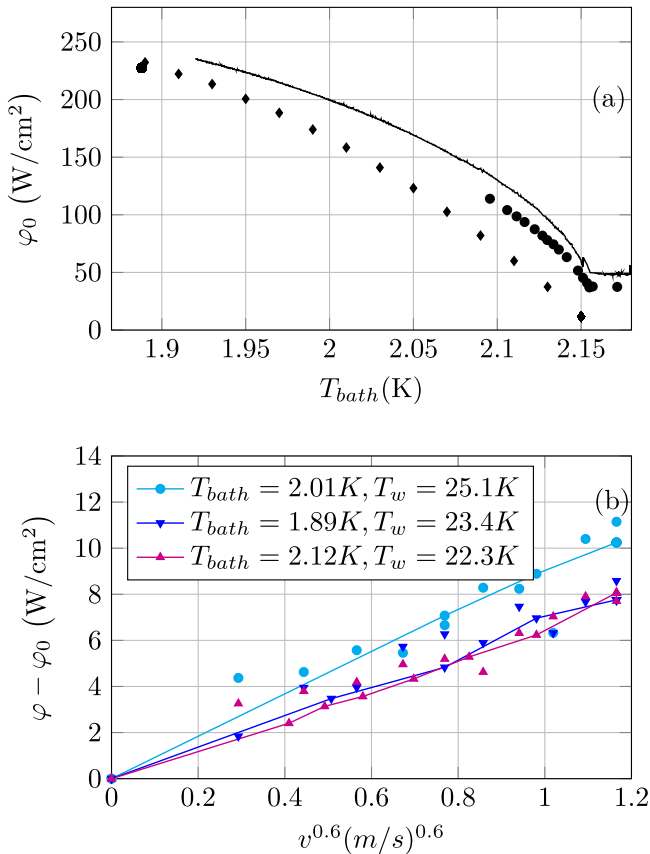


FIG. 1. (a): Average heat flux at the surface of a hot wire of size $D_w = 1.3 \mu\text{m}$ operated at $T_w \approx 21 \text{ K}$ at null velocity. Continuous line: time series during cooling of the bath, obtained using a constant-resistance CTA electronics. Circles (\bullet): open loop constant voltage measurements (see text). Diamonds (\blacklozenge): Numerical integration of the model based on conduction function. (b): additional heat flux due to He II forced convection, represented as a function the power 0.6 of the velocity. The points that are linked by a line are the result of a 30 times longer averaging and their temperature is controlled much more carefully than unlinked points.

shown here), $\alpha = 0.5$ is well suited, in He II case, a value $\alpha = 0.6$ gives a slightly better fit (see Figure 1(b)).

The probe response in He-II and its similarity with the response of classical hot wires are first indications that hot wires can be operated as velocity probes in He-II. Still, heat transfer processes occurring near the wire surface are more complex—as discussed later—and no clear justification can be brought about the slight change in the scaling with the mean flow velocity. Consequently, we have decided to analyze time series data of the raw CTA output $e(t)$ rather than attempting to use Eq. (2) to convert it into velocity time series. Since $\varphi \sim e(t)^2$ and $\varphi - \varphi_0 \ll \varphi_0$, the fluctuations of the raw signal $e(t)$ are nearly proportional to the heat flux $\varphi - \varphi_0$.

B. Power spectra from the hot-wire

Figure 2 presents the power spectral density (PSD) of the voltage e delivered by the hot wire electronics, normalized by its variance σ_e^2 :

$$E^*(f) = E(f)/\sigma_e^2, \quad (3)$$

where E , the PSD of the voltage signal, is computed using Welch periodogram method over windows of 2^{16} points. The

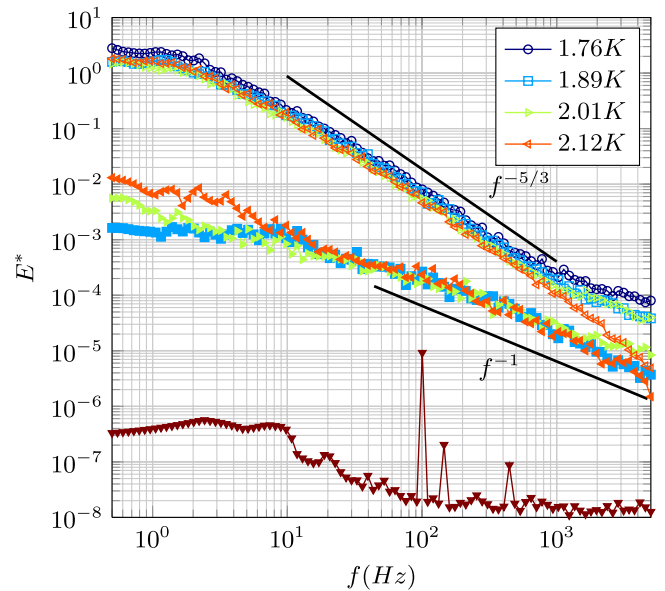


FIG. 2. Power spectral density of the CTA electronics output voltage normalized by its variance, for a flow velocity $U_{60D} = 1.3 \text{ m s}^{-1}$ (open symbols) at four temperatures. The corresponding colors with filled symbols correspond to the same temperature but at null velocity. In the latter case, the signal is normalized by the variance of the signal at non-null velocity. Pointing down triangles show the observed noise in He I (the corresponding non-null velocity spectrum is not shown here).

PSD at four different temperatures, ranging from 1.76 K up to 2.12 K ($T < T_\lambda$), are represented as a function of the frequency for a mean flow velocity $U_{60D} = 1.3 \text{ m s}^{-1}$ on the wire. Null jet velocity PSD are represented (filled symbols) normalized by the variance of their corresponding non-null-velocity signal. For comparison, the normalized PSD at null jet velocity in He I is also represented (pointing down triangles).

The first observation is that the null velocity “noise” has a much higher level of fluctuations in He II than in He I.

At non-null jet velocities, a Gaussian white PSD is observed up to $f \approx 2 \text{ Hz}$. This is consistent with the expected incoherent motion of the very large scales of the flow. For higher frequencies, the PSD exhibits a power law behavior consistent with Kolmogorov $f^{-5/3}$ scaling. A departure from this power law is observed at frequencies of order $f \approx 2 \text{ kHz}$, except at temperatures close to T_λ : the PSD decreases much less rapidly (roughly as $f^{-0.5}$). As can be seen, at the highest resolved frequencies, the energy density of the signal is always higher than the one observed at null velocity.

The observation of a plateau followed by a Kolmogorov-like spectra in He-II is a second indication that the hot wire is sensitive to velocity fluctuations, at least up to 2 kHz. Indeed, such spectral behavior has already been reported in He-II flows (e.g., Refs. 5–7) and their observation is known to be robust to non-linearities in the calibration law.

C. Correlation with a Pitot tube anemometer

A Pitot-tube anemometer working both in He-I and He-II was specially made to test the correlation between the raw hot-wire signal and velocity fluctuations. It is mounted close to the hot-wire, at a 4 mm transverse distance and 3 mm

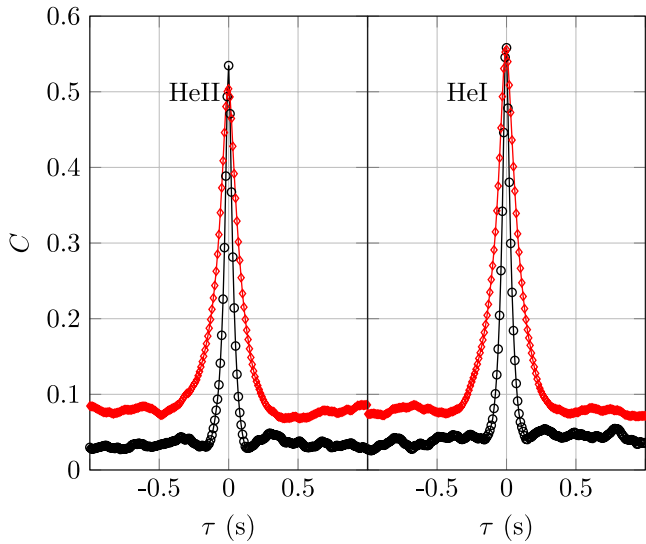


FIG. 3. Cross-correlation coefficient of the hot wire signal and of a total head pressure tube situated 4 mm apart (black \circ 1.72 m/s and red \diamond 0.86 m/s). Measurements are performed at $45 D_n$ from the nozzle.

downstream of it. Its design is based on those found in Ref. 6. Figures 3(a) and 3(b) present the cross-correlation $C(\tau)$ of the Pitot anemometer raw electrical signal $v(t)$ with the hot wire CTA raw output signal $e(t)$ both in He-I and He-II, where

$$C(\tau) = \frac{\langle (e(t) - \langle e \rangle)(v(t + \tau) - \langle v \rangle) \rangle}{\sigma_e \sigma_v},$$

σ_e and σ_v being the root-mean-squared values of the signals.

In He-I, both probes are known to measure velocity. The maximum value of C at small time lag, about 55% is not expected to be 100% because the hot-wire signal is not calibrated and its calibration curve is not expected to be linear. Furthermore, the noises of the sensors that have a non-hydrodynamic origin, are not expected to be correlated and will naturally decrease the correlation coefficient of the signals.

The most striking result is to obtain nearly the same level of correlation in He I and in He II. This gives a strong indication that the most energetic velocity fluctuations of the flow are producing similar response of the hot-wire in He-I—where it is a validated anemometer—and in He-II.

IV. DISCUSSION

A. Response without external flow

Due to the 21 K operating temperature of the hot wire, the liquid helium in the vicinity of the wire surface is in the supercritical normal phase (noted He I hereafter for simplicity), while far from the wire, helium is in the He-II phase. These near-wire and far-wire regions are separated by an isotherm interface at T_λ . In the absence of external flow, we will first assume that the temperature distribution has a cylindrical symmetry, r_λ being the radius of the T_λ isotherm.

In the cylindrical shell of He-I surrounding the wire, molecular conduction is responsible for most of the heat transport.²³ For a typical heat flux of $\varphi_0 = 100 \text{ W cm}^{-2}$, numerical integration of Fourier law between $T_w \approx 21 \text{ K}$ (at $r = D_w/2$) and $T_\lambda \approx 2.15 \text{ K}$ (at $r = r_\lambda$) gives a He-I shell layer

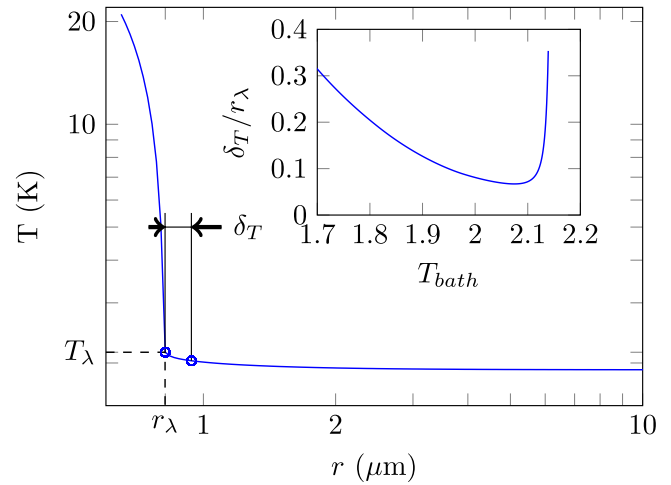


FIG. 4. Typical radial temperature profile around the wire, computed for $T_{bath} = 1.91 \text{ K}$. Inset: Thermal boundary layer in He II δ_T normalized by r_λ , the radius of He I region.

thickness of $r_\lambda - D_w/2 \approx 0.2 \mu\text{m}$. Although Fourier law may not be accurate over such small distances and considering the very large temperature gradient, it still provides an estimate and shows that the He-I shell surrounding the wire is significantly thinner than the wire diameter.

In the far-wire region, molecular conduction is complemented by the counterflow heat transport mechanism, specific to He-II.¹ At scales larger than the typical inter-vortex spacing, the overall mean heat flux in He-II is given by

$$\tilde{\varphi} = (f(T, P)^{-1} \nabla T)^{1/m}, \quad (4)$$

$m \approx 3$ is the so-called Gorter-Mellink exponent (it was shown that $m = 3.4$ generally leads to better fits of experimental data^{24,25}) and $f(T, P)^{-1}$, called the conduction function, is a highly temperature and pressure dependent quantity which is null at T_λ and maximum at 1.93 K in our experimental conditions.

The efficient heat transport brought by the counterflow mechanism (Eq. (4)) results in significantly smoother temperature gradients in He-II than in He-I (Figure 4). The inset in Figure 4 illustrates the dimensionless thermal boundary layer thickness δ_T/r_λ defined as $T(r_\lambda + \delta_T) = (T_{bath} + T_\lambda)/2$. As can be seen, the thermal boundary layer extends over a typical distance $\delta_T \approx r_\lambda/5 \approx D_w/10$.

The conduction function is generally used for systems in which the heat flux is lower than in this experiment. In our case, the very high heat flux leads to counterflow velocities $v_n - v_s = \tilde{\varphi}/\rho_s S T$ that can be of order of the second sound velocity near the wire. For this reason, quantities extracted from the classical literature must be applied to our case with caution. However, it is interesting to use experimental (e.g., Tough²⁶ and references there in) and numerical (e.g., Schwarz²⁷) fits to estimate the superfluid vortex line density $\mathcal{L}_0(r)$ sustained by the counterflow. Neglecting the mean velocity of the vortices in the tangle, the vortex line density can be estimated as:

$$\mathcal{L}_0 = a(v_n - v_s)^2 \quad (5)$$

where a is a temperature dependent parameter. Using numerically computed values²⁷ of a , the maximum of \mathcal{L}_0 is found at $r = r_\lambda$ and represents an inter-vortex spacing of order $r_\lambda/50 \approx D_w/100$. This indicates that close to the wire, the inter-vortex spacing is much lower than the wire diameter. In first approximation, the time averaged vortex line density can be approximated as a continuous field at the wire diameter length scale, which thus justifies *a posteriori* the use of a continuous model to derive order of magnitude estimates.

Numerical integration of the model in He-I and He-II is done in cylindrical coordinates using Dirichlet boundary conditions

$$\begin{cases} T = 21 \text{ K} & \text{for } r = D_w/2 = 0.65 \mu\text{m} \\ T = T_{bath} & \text{for } r = 1000D_w. \end{cases}$$

In Figure 1(a), we have represented experimental (line and circles) and numerical (diamonds) heat flux φ_0 at the surface of the wire, as a function of the bath temperature T_{bath} . For temperatures well below T_λ , we find that our simple model accounts reasonably well both for the order of magnitude and temperature dependence of heat flux, showing that the underlying phenomena are mainly driven by the counterflow mechanism. This is consistent with the previous studies with heated micro-wires,^{28,29} although they were done with wires with diameters 40–60 times larger. For bath temperatures T_{bath} close to T_λ , our model predictions are underestimated by typically 50 W cm^{-2} . Since this offset is also present right above T_λ , it is not He-II related and its origin has not been examined in detail. Possible origins include thermal end-effect associated with the prongs or residual offset introduced by the circuitry. It should also be stressed out that the accuracy of our numerical simulation depends on the accuracy of the data we use for the conduction function: for a given temperature gradient, the computed flux using Hepak[®] library (used for the numerical integration above) and correlations by Sato *et al.*²⁴ differ by up to a factor of ~ 2 for large heat fluxes.

As a final remark, the observed heat flux without external flow in He II is a time dependent quantity, as illustrated by the PSD of Figure 2 (filled symbols). Over 2-3 decades, a f^{-1} power law roughly fits the spectra. The fluctuating behavior of the heat flux in counterflows was studied by various authors (for a review, see Ref. 30), and the cause of fluctuations is understood as turbulent nature of the counterflow.³¹

B. Response to an external flow

In the previous section, we have presented three experimental results that can be interpreted stating that hot-wires can provide a direct measurement of velocity in He-II. Before discussing the velocity dependence, we first discuss (and finally discard) two alternative interpretations, namely, the sensitivity to temperature fluctuations and to the vortex line density present in the external flow.

As stated above, the temperature sensitivity is of order $\tilde{\gamma} \approx -2 \text{ K}^{-1}$. For the temperature driven fluctuations to contribute significantly to the measured signal, the temperature rms fluctuations δT should be of order $\delta T = (\varphi(v) - \varphi_0)/(\varphi_0 \tilde{\gamma})$

$\approx 30 \text{ mK}$ at the largest measured velocities. Such large temperature fluctuations are not likely to happen in our flow :

- At large time scales, i.e., for frequencies smaller than 10 Hz, the temperature controller maintains the temperature within $\pm 0.1 \text{ mK}$. Furthermore, the correlation between the velocity and the temperature at large time scale is expected to be null because of the very efficient thermal transfer associated with He II.
- For smaller time scales, the local energy dissipation could produce temperature fluctuations but their order of magnitude would be much smaller. A higher bound for the dissipated energy by unit mass may be computed using the pressure loss through the nozzle which gives the maximum achievable temperature fluctuations in the flow : $\theta'_{max} = V_{nozzle}^2/2Cp \approx 10 \text{ mK}$, where Cp is the constant pressure specific heat of helium. Once again the efficient thermalization of the flow due to the counterflow prevents any such high temperature fluctuations at small time/length scales.

Thus, the temperature effect on the hot wire signal can reasonably be neglected, at least for the low frequency part of the signal.

Now the vortex line density \mathcal{L} of the turbulent external flow could possibly contribute to the hot wire signal. Indeed, as mentioned earlier, the vortex lines are the basic ingredient limiting the heat flow in the counterflow surrounding the wire, and one could argue that the time-dependent vortex lines carried by the external flow will add up to the intrinsic vortex lines generated by the counterflow. Here, again two main arguments lead us to discard the relevance of this mechanism:

- The mean vortex spacing $\delta = \mathcal{L}^{-1/2}$ was found to behave similarly with the Kolmogorov dissipative scale in classical turbulence,^{32,33} i.e., \mathcal{L} increases with the Reynolds number as $Re^{3/2}$ and thus with velocity. This leads to the conclusion that a higher mean velocity would lead to a degraded heat transfer, which is obviously opposite to the observation of Fig. 1(b).
- Both references cited above provide correlations between δ and the Reynolds number. In our conditions $\delta \approx 3 \mu\text{m}$ which is more than 100 times larger than the estimated value near the wire. The vortex line density of the external flow is much sparser than the one produced by the thermal counterflow near the wire.

To discuss the velocity dependence, we first come back to the calibration law Eq. (2). Obviously the term φ_0 accounts for the heat flux at null velocity. In classical fluids this term is mainly due to natural convection whereas in He-II, it is due to the counterflow mechanism, as seen previously. Contrary to the classical case, this null-velocity term in He-II is found to remain dominant over the advection term ($\varphi_0 \gg Bv^\alpha$), even in the presence of a vigorous flow slightly exceeding 1 m s^{-1} . Thus, it is reasonable to assume that the flow alters only slightly the underlying counterflow heat transport mechanism in most of the He-II fluid domain. A self consistency test of this assumption can be performed by estimating the local Péclet number defined as the ratio of the advection and counterflow

terms

$$Pe(r) = \frac{\rho c_p v (T(r) - T_{bath})}{(f(T, P)^{-1} \nabla T)^{1/m}}, \quad (6)$$

where ρc_p is the volumetric heat capacity.¹ Numerical integration shows that Pe remains smaller than one, in agreement with our assumption.

Solving the steady heat equation in He-II at null velocity gives $T(r) - T_{bath} \sim r^{1-m}$ for $r \gg r_\lambda + \delta_T$ (where $f(T, P)$ can be taken constant). Due to this pronounced power law decay ($1 - m < -1$), the heat advected by the external flow in the far-wire region is small compared to the one advected in the wire vicinity, as can be seen by integration of the numerator of the $Pe(r)$. Thus, the velocity dependence of the heat transfer must originate from the near-wire region, say within few $r_\lambda + \delta_T \approx 1 \mu\text{m}$ from the wire axis. This analysis justifies the sensitivity to local fluctuations of the velocity, a key property of classical hot wires. We stress that this conclusion is obtained without making assumption on the physical mechanisms at play very close to the wire.

Modeling what happens in the micron-size region which surrounds the wire and understanding the resulting velocity dependence is delicate and is beyond the scope of this experimental work. Difficulties arise because this near-wire region embraces a He-I classical fluid domain surrounded by the He-II superfluid and on top of both the velocity boundary layer produced by the incoming flow impinging the wire. Additional technical difficulties arise from the strong fluid property variations in space, a possible breakdown of the validity of the continuous model, as well as a spatial cross-over from a radial counterflow around the wire to a translational motion of He-II away from it.

As a final comment, we want to stress the small—if any—temperature dependence of the advection term Bv^α in the hot-wire calibration (see Fig. 1(b)). This experimental result is very constraining for model development. For example, it undermines a straightforward modeling approach consisting in considering advection as an independent heat transport mechanism which adds up to an underlying counterflow transport. Indeed, simple models elaborated along this line by integrating the advection term $\rho c_p v (T(r) - T_{bath})$ using a classical velocity boundary layer successfully predict a $\sim v^{0.5}$ velocity-dependent heat transfer around the hot-wire but over-estimate significantly the temperature dependence of the advection term.

V. CONCLUSION

We have brought three experimental observations, and presented quantitative arguments, that show that a hot-wire can be used as a local velocity sensor in He II turbulent flows.

We showed that the calibration law (against the mean velocity) shares some common scalings with the one observed in classical fluids. The good correlation of the hot-wire signal with a validated local velocity sensor together with the $f^{-5/3}$ scaling of the power spectra are further indications that the response of the hot-wire in He II is mainly related to the local velocity of the fluid.

The microscopic mechanisms near the surface of the wire when submitted to an external flow are delicate to analyze for a number of reasons: the large density variation in the He I layer and the very high counterflow velocity in He II (of order of the second sound velocity) very close to the wire. Still, the heat transport properties are well-know further away from the wire, thanks to the $1/r$ decrease of the heat flux density. Using these properties, we could justify that the observed velocity dependence originates in the near vicinity of the wire, within typically one micron. Thus, the very high effective conductivity of He-II does not spoil the spatial resolution of the sensor which is therefore given by the length of the wire.

Although further studies are needed to understand the microscopic physics at play within the micron-thick shell surrounding the hot-wire, such probe can already be counted as local velocity sensor in superfluid helium, in the 1 m/s velocity range.

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